

Improving control over losses and tank emissions though your Production Accounting data

Overview

Evaporation from fixed and floating roof storage tanks is a major source of product loss in the crude oil industry. Evaporation losses should be minimized to help maximize company revenue, meet regulatory

requirements, and reduce greenhouse gas emissions. The accurate quantification of evaporative losses from storage tanks is imperative given the impact to the company's bottom line and the environment. Emissions from storage tanks consist of working losses and breathing losses.

Several international institutes have published detailed methods for calculating losses from storage tanks. However, these methodologies are tedious and time-consuming to the occasional user.

VM-PA[™] Storage Tanks Evaporation Losses

VM-PA incorporates the calculation for storage tank emissions. These emission calculations use equations

derived from an August 2001 CEP article by Jimmy Peress. These equations apply for fixed roof tanks and typically deliver results which are usually within 10% of the methodology used by the EPA Tanks 4.09 program.

The VM-PA standard mass loss report is built following the best practices announced by the HM-31 Standard by the Energy Institute¹. In this line, the Accounted Loss table has been recently added to the VM-PA mass losses report to comply with the HM-31 recommendation: "In order to assist in understanding the variation and reduce loss, it is important to identify known sources or potential sources and one method for this is to construct the Accounted Loss Table. This tables assists good control by identifying changes and allows the refinery to monitor the potential sources of loss and quantify the amount as far as is possible by measurement or calculation or a mixture of both."

Mass losses			VISUALMESA [™]
Model: DM-SITE - Demo Model - Site From: 02/01/2011 00:00:00			PRODUCTION ACCOUNTING
Fo: 03/03/2011 23:59:59			
Using: Measured quantities			
User: Site accountant/das			
Report type: Summary			
BC-SITE - Balance control - Site	4 >	Outlets + Consumptions	
Processed charges	(kg)	Outlets + Consumptions	(kg
Receipts - Refinery		Shipments - Balance	
00. Gas	21,733,069	20. Liquified Gas	25,206,93
10. Crude	475,976,657	35. Finished Naphta	144,429,28
20. Liquified Gas	3,318,883	55. Finished Distillates	167,229,22
35. Finished Naphta	9,294,060	60. Heavy Distillates	128,834,95
40. Naphtha Additives	7,009,445	70. Solids	42,999,62
55. Finished Distillates	3,008,597	Subtotal	508,700,02
Subtotal	520,340,711	Consumptions - Refinery	
Inlets - Refinery		00. Gas	18,072,81
80. Miscellaneous	4,910,014	60. Heavy Distillates	5,087,86
Subtotal	4,910,014	Subtotal	23,160,67
Charges inventory		Materials inventory	
Initial inventory	100, 115, 214	Initial inventory	32,751,66
Final inventory	82,059,244	Final inventory	36,756,59
Inventory difference	18,055,970	Inventory difference	4,004,92
Total processed charges	543,306,695	Total Outlets + Consumptions	535,865,62
Losses results summary	7.441.071	Accounted losses table	% total % inpu
Accounted losses	12,105,305	Flaring	233,576 3.14 0.0
Unaccounted losses	-4.664.234	Losses from API Separator Evap	1.107.563 14.88 0.2
	1.37	Tank evaporation losses	10.764.166 144.66 1.9
% Total losses			



¹ HM-31 Guide to Hydrocarbon Management in Petroleum Refinery Operations, Energy Institute, London, UK.

